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Reduction of surface area of lignin improves enzymatic hydrolysis of cellulose from hydrothermally pretreated wheat straw

M. H. Sipponen,* V. Pihlajaniemi, O. Pastinen and S. Laakso

Enzymatic hydrolysis of cellulose after pretreatment of wheat straw (WS) was investigated for the first time in relation to lignin surface area (SA). Lignin SA in solid residues from WS autohydrolysis (AH) and successive NH_3 (aq) extraction was determined using cationic dye adsorption. AH at increasing severity decreased up to 45% and 53% of WS lignin SA and specific surface area (SSA), respectively. Cellulose-to-glucose conversion from AH solid fractions from 24 h reaction with 15 FPU g^{-1} cellulase activity increased linearly from 31% to 91% with decreasing lignin SA. When AH solid fractions were extracted with NH_3 (aq), both lignin SA and SSA increased in the corresponding solid residues, SSA up to 92%. As a consequence, cellulose-to-glucose conversion decreased in spite of the lower proportion of lignin in the solid residues after the NH_3 (aq) extraction. Up to 85% sugar yield was obtained from the single-stage AH process but when combined with NH_3 (aq) extraction the two-stage process yielded at most 71% of the original straw sugars. These results show that, independent of the lignin content, reduction of surface area of lignin improves the enzymatic hydrolysis process.

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Introduction

Production of biofuels from renewable lignocellulosics is complicated by lignin that impedes enzymatic hydrolysis of carbohydrates. Without pretreatment, lignin content of forages shows a negative linear correlation with digestibility.¹ The detrimental effect of lignin on enzymatic hydrolysis of carbohydrates has been attributed to inhibition of enzymes by lignin,² unproductive adsorption of cellulases on lignin,³ and steric hindrance caused by lignin or lignin-carbohydrate complexes to cellulases.^{4,5}

Hydrothermal pretreatments that reduce recalcitrance of lignocellulosic biomass to enzymatic hydrolysis do not normally decrease lignin content in the solid fraction. Instead, enrichment of lignin occurs particularly as a result of hemicellulose dissolution in a process referred to as autohydrolysis (AH).⁶ AH cleaves lignin-carbohydrate linkages, and consequently improves enzymatic hydrolysis of cellulose. Lignin has been said to undergo both depolymerization and repolymerization,⁷ the first resulting from cleavage of aryl ether bonds under acidic conditions.⁸ Although degradation of cellulose does not usually occur in AH,⁷ hemicellulose degradation can be drastic. The degradation products take part in further reactions, which in acid-catalyzed conditions generate so-called pseudo-lignin⁹ that has been suggested to impede enzymatic hydrolysis of pretreated lignocellulosics.¹⁰ Previously, the amount of pseudo-

lignin in the aqueous ammonia extracts from wheat straw (WS) AH solid residues increased linearly with increasing AH severity.¹¹ It might thus be difficult to avoid generation of pseudo-lignin completely if high enzymatic hydrolysis yield from the solid residues is desired. However, increased enzymatic carbohydrate conversion after AH at high severity has been reported in spite of droplets of altered lignin observed on WS.¹²

The effect of lignin on enzymatic hydrolysis process after AH is not yet fully understood. Here, the key questions are whether formation of surface deposited pseudo-lignin is detrimental altogether, and could enzymatic hydrolysis of cellulose be improved by removal of pseudo-lignin from AH solid residues. In the current paper, WS solid residues from AH only, or with successive NH_3 (aq) extraction were characterized for composition and surface area (SA) of lignin. The determination of lignin SA was made according to the newly developed method that is based on specific adsorption of the cationic dye Azure B on lignin.¹³ Changes in lignin SA and specific surface area (SSA) revealed the effect of AH severity on lignin. For the first time, the lignin SA was correlated to enzymatic hydrolysis of cellulose. Discussion of the results opens up a new perspective for the investigation of existing and novel lignocellulose fractionation processes.

Experimental

Fractionation of wheat straw by autohydrolysis and aqueous ammonia treatments

Preparation of the solid residues from WS AH treatment and successive aqueous ammonia extraction has been described

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Fig. 1 Scheme of the studied alternative processes for fractionating wheat straw.

elsewhere¹¹ and outlined in Fig. 1. Briefly, AH was conducted at 170–200 °C maximum temperature and a part of the solid residues was extracted with NH_3 (aq) either at moderate intensity (140 °C, 5% NH_3) or high intensity (160 °C, 20% NH_3) conditions. The solid residues were separated by filtration, washed until neutrality, and stored at 4 °C until enzymatic hydrolysis experiments.

Analytical procedures

Analytical results were calculated based on dry matter content of the sample, as determined gravimetrically by drying at 105 °C to constant weight. The analytical determinations were carried out in duplicate, and the mean values were calculated.

Compositional analysis

The solid lignocellulose fractions were milled using a type Pulverisette 14 mill (Fritsch, Germany) to pass through a 200 μm screen prior to the two-stage sulfuric acid hydrolysis.¹⁴ Gravimetric analysis of the acid-insoluble residue, isolated by filtration on a Whatman GF/F membrane and corrected for its ash content gave a fraction termed Klason lignin. Monosaccharides were analyzed from the sulfuric acid filtrate after neutralization with CaCO_3 by high-performance liquid chromatography (HPLC) using the system described in the literature.¹⁵

Enzymatic hydrolysis of solid residues from wheat straw

Enzymatic hydrolysis of solid residues (0.5 g) was performed in 100 mL conical flasks at 2% solids concentration (w/v) in 50 mM sodium phosphate buffer (pH 4.8). Reactions catalyzed by an enzyme mixture containing 15 FPU g^{-1} Econase CE cellulase preparation (AB Enzymes, Finland) supplemented with cellobiose preparation Novozym 188 (Novozymes, Denmark) at 81 CBU g^{-1} , and GC 140 xylanase preparation (Genencor, Denmark) at 1020 IU g^{-1} were carried out in an oscillation (100 rpm) water bath (B.Braun, Germany) at 50 °C. Enzyme activities were determined according to literature.^{16,17} One activity unit (U) refers to the amount of the enzyme that releases 1 μmol of glucose or xylose under the assay conditions. Tetracycline (0.04 mg mL^{-1}) and cycloheximide (0.03 mg mL^{-1}) were used to inhibit bacterial growth. Hydrolysis was followed by sampling at 24 h and 72 h for sugar analysis. Hydrolysis yield and sugar yield were calculated using the following formulae:

$$\text{Hydrolysis yield (\%)} = 100\% \cdot m_{\text{sugar, EH}} / m_{\text{SR}}$$

$$\text{Sugar yield} = [m_{\text{sugar, AH}} + Y_{\text{SR}} \cdot \text{Hydrolysis yield (\%)}] / (m_{\text{WS}} \cdot 0.741)$$

Here, $m_{\text{sugar, EH}}$ (g) is the total amount of monosaccharides released in enzymatic hydrolysis of the solid residue sample (m_{SR}), $m_{\text{sugar, AH}}$ (g) is the total amount sugar (as monosaccharides) released from WS in AH, Y_{SR} (%) is the yield of solid residue from either AH only, or with successive extraction with NH_3 (aq) relative to the amount m_{WS} (g) of WS weighed to AH, and 0.741 is the proportion monosaccharides released in analytical acid hydrolysis of WS as described in 2.2.1.

Characterization of lignin surface area by Azure B adsorption

Surface area of lignin (SA) and specific surface area of lignin (SSA) were determined according to the literature.¹³ Briefly, solid residues (100 mg) were agitated in 0.1 g L^{-1} Azure B solution at pH 7 at 25 °C, and after 24 h the absorbance was measured from the liquid phase passed through 0.45 μm PTFE filters. Lignin surface area (SA) and specific surface area (SSA) were calculated based on the amount of surface-accessible acidic hydroxyls:

$$\text{Lignin SA} = \left(\frac{\text{mmol}}{\text{g}} \right) = 0.91 F_{\text{WS}} \frac{1.64 q_e}{305.83} \cdot 397$$

$$\text{Lignin SSA} = \left(\frac{\text{m}^2}{\text{g lignin}} \right) = \text{SA} / \text{proportion of lignin}$$

Here, 0.91 is a correction factor for non-specific binding, F_{WS} is the correction factor based on the total lignin content of the solid fraction, 1.64 is the ratio of maximum equilibrium adsorption capacity to equilibrium adsorption capacity of WS in the assay conditions, q_e is the equilibrium adsorption capacity of solids residues in the assay conditions, 397 ($\text{m}^2 \text{mmol}^{-1}$) is the area covered by Azure B, and proportion of lignin (%) is the

Table 1 Klason lignin (KL), acid-soluble lignin (ASL), and carbohydrate contents of wheat straw (WS) and solid residue fractions obtained from treatments outlined in Fig. 1^a

Solid fraction	Treatment severity ^b	KL (%)	ASL (%)	Glucose (%)	Xylose (%)	Arabinose ^c (%)	24 h Cellulose conversion (%)
WS	—	21.8 ± 0.2	1.8 ± 0.0	39.8 ± 0.2	23.5 ± 0.4	2.7 ± 0.0	14.7 ± 0.8
170C _a	3.10	22.1 ± 0.2	1.3 ± 0.1	41.2 ± 0.6	21.9 ± 1.1	2.1 ± 1.0	31.8 ± 0.2
170C _b	3.15	21.5 ± 0.1	1.3 ± 0.0	41.5 ± 0.8	23.7 ± 0.1	1.8 ± 0.3	31.2 ± 0.1
180C _a	3.47	23.1 ± 0.0	1.2 ± 0.1	47.2 ± 2.1	19.3 ± 1.5	1.5 ± 0.8	40.9 ± 0.4
180C _b	3.52	23.2 ± 0.1	1.1 ± 0.0	47.2 ± 1.5	18.5 ± 0.1	0.8 ± 0.4	45.4 ± 0.4
190C _a	3.81	24.8 ± 0.1	0.9 ± 0.0	52.1 ± 1.8	11.1 ± 0.7	1.3 ± 0.7	70.4 ± 2.4
190C _b	4.06	28.2 ± 0.1	0.9 ± 0.0	56.3 ± 2.1	7.7 ± 0.6	0.6 ± 0.6	76.9 ± 0.6
195C	4.10	24.6 ± 0.0	0.9 ± 0.1	53.6 ± 1.8	4.2 ± 0.4	nd ^d	89.3 ± 0.6
200C	4.39	26.3 ^e	1.0 ^e	55.3 ^e	2.9 ^e	nd	91.5 ± 1.9
M170C _b	M ^f	18.2 ± 0.1	1.0 ± 0.1	50.4 ± 1.3	19.9 ± 0.8	1.5 ± 0.1	66.5 ± 1.0
M180C _a	M	19.3 ± 0.2	1.1 ± 0.0	55.6 ± 0.9	15.0 ± 0.1	0.5 ± 0.1	53.3 ± 0.0
M190C _a	M	20.4 ± 0.1	0.8 ± 0.1	65.2 ± 0.4	9.3 ± 1.0	1.6 ± 0.2	64.3 ± 1.7
M195C	M	22.1 ± 0.0	0.6 ± 0.0	67.6 ± 2.0	3.9 ± 0.1	0.7 ± 0.1	72.3 ± 1.2
M200C	M	24.0 ± 0.0	0.5 ± 0.0	67.0 ± 1.6	3.2 ± 0.8	0.9 ± 0.3	66.4 ± 0.3
H170C _a	H ^g	14.6 ± 0.2	1.0 ± 0.0	61.0 ± 1.1	17.9 ± 0.5	0.8 ± 0.0	69.3 ± 1.6
H180C _a	H	12.1 ± 0.2	0.9 ± 0.0	66.8 ± 2.2	15.0 ± 0.4	0.8 ± 0.5	78.7 ± 1.4
H190C _a	H	12.7 ± 0.0	0.7 ± 0.0	72.5 ± 4.0	9.0 ± 0.3	1.0 ± 0.2	84.7 ± 1.1
H195C	H	15.2 ± 0.2	0.7 ± 0.0	74.2 ± 3.3	4.4 ± 0.2	0.3 ± 0.3	79.4 ± 1.7
H200C	H	20.3 ± 0.2	0.6 ± 0.0	70.7 ± 1.2	2.1 ± 0.1	0.9 ± 0.5	60.1 ± 0.2

^a KL, Klason lignin; ASL, acid-soluble lignin. The content of glucose, xylose and arabinose are expressed as anhydrous sugars. The amount of galactose in the solid residues (not shown) was less than one percent. ^b Autohydrolysis severity was calculated from $\log R_0 = \log[t \times \exp[(T - T_{ref})/14.7]]$ (Overend and Chornet, 1987). ^c Analyzed as sum of arabinose plus mannose. ^d nd, not detected. ^e Values from single determination. ^f M, moderate intensity extraction (5% NH₃ (aq), 140 °C). ^g H, high intensity extraction (20% NH₃ (aq), 160 °C). The values after ± indicate average deviation from the mean values.

sum of Klason lignin and acid-soluble lignin contents in the solid residues.

Results and discussion

Effect of autohydrolysis and aqueous ammonia treatments on solid residues

Composition and appearance of straw solid fractions from AH and NH₃ (aq) treatments was investigated in order to reveal changes in proportions of carbohydrate and lignin components. Both of the treatments removed hemicelluloses from the straw solids, and after the most severe AH only 2.9% xylan remained in the solid residues (Table 1). Due to partial dissolution of both lignin and hemicellulose, NH₃ (aq) extractions enriched cellulose content in the solid residues to 68% and 74% after moderate (M) and high (H) intensity extractions, respectively. The maximum reduction in Klason lignin content (49%) was obtained from AH solid fractions produced at $\log R_0 = 3.81$ compared to 23% reduction at $\log R_0 = 4.39$. At higher severities ($\log R_0 \geq 4.10$) accumulation of pseudo-lignin and formation of condensed lignin could explain the increasing amount of lignin in the solid fraction and its resistance against NH₃ (aq) extraction. This biphasic behavior with respect to AH severity has previously been shown only for wood materials.¹⁸ Therefore, possible structural changes in WS lignin that may have occurred in AH and NH₃ (aq) extraction were studied more closely.

Visual observation revealed that AH had produced dark brown matter, which may have originated from relocalization of lignin from disrupted lignin-carbohydrate network onto

particle surfaces and by formation of surface-deposited pseudo-lignin. SEM micrographs confirmed the presence of spheres on AH solid fractions (Fig. 2). Physical fluidization of lignin by melting at temperatures above its glass-transition temperature may have caused aggregation and formation of denser material that precipitated on solid surfaces. Only the high intensity NH₃ (aq) extraction removed the spheres from the solid residues (Fig. 2), consistent with their lower lignin content than after the

Fig. 2 Scanning electron micrographs of untreated wheat straw (1-a to 1-c) and solid residue fractions of straw obtained from autohydrolysis at 190 °C before (2-a to 2-b) and after NH₃ (aq) extraction in moderate (3-a to 3-c) and high (4-a to 4-c) severity conditions.

moderate intensity extraction (Table 1). Previously, presence of lignin-containing droplets was shown in micrographs of solid residues from dilute acid treatment of maize stalk.^{19,20} Ahead of the current study the proportion of pseudo-lignin in the NH_3 (aq) extracts from the AH solid residues was estimated to be as high as 55%.¹¹ However, altered lignin has not been quantified in the AH solid residues, and its effect on enzymatic hydrolysis or surface area of lignin has not been elucidated before.

Effect of autohydrolysis and NH_3 (aq) extraction on specific surface area of lignin

Native WS lignin is expected to undergo structural changes in the pretreatment conditions. Effect of AH and NH_3 (aq) extractions on lignin structure was studied by cationic dye adsorption in order to estimate possible changes in surface area (SA) of lignin. Azure B is a basic violet-blue dye that leaves lignin-free tissues unstained,²¹ but instead binds to acidic hydroxyl groups of lignin.¹³ Increasing severity ($\log R_0$) decreased lignin SA of the AH solid residues from 84 m^2 of the untreated straw to 47 m^2 after the highest AH severity (Fig. 3a). In contrast, moderate intensity NH_3 (aq) extraction (5% NH_3 , 140 °C) increased lignin SA compared to the corresponding AH solid residues. However,

the high intensity NH_3 (aq) extraction (20% NH_3 , 160 °C) decreased lignin SA at severities up to $\log R_0 = 3.81$. These differences in lignin SA are in accordance with the earlier results that showed higher relative proportion of pseudo-lignin in the aqueous ammonia extracts from the moderate intensity extraction than from the high intensity extraction.¹¹ As a result of the moderate intensity NH_3 (aq) extractions that dissolved higher proportions of pseudo-lignin, the resulting solid residues were enriched in lignin containing acidic hydroxyl groups. This is also indicated by only slight decreases in the lignin content of the solid residues after moderate intensity extraction (Table 1).

When surface area of lignin was calculated relative to the proportion of lignin in the solid residues, lignin specific surface area (SSA) decreased linearly as a function of AH severity (Fig. 3b). Compared to the lignin SSA of AH solid residues, NH_3 (aq) extraction increased the lignin SSA of the corresponding solid residues, high intensity extraction more than moderate intensity extraction. These results indicate that AH had drastic overall effect on surface properties of lignin in solid residues obtained at $\log R_0 \geq 4.1$, showing lignin SSA that were less than half than in untreated WS (354 $\text{m}^2 \text{g}^{-1}$). Although these changes could be attributed to lignin repolymerization reactions that form non-labile biphenyl ether (5-O-4) structures, SEM investigation of the straw solid residues and compositional analysis of the aqueous ammonia extracts suggested that phase transition of lignin (melting) and accumulation of pseudo-lignin were the main changes causing lower lignin SSA. Removal of pseudo-lignin could be conducted using NH_3 (aq) that dissolves it more selectively than native lignin from the AH solid residues,¹¹ thus exposing acidic OH groups of lignin on the surfaces. Previously, supplementation of cellulose with artificially generated pseudo-lignin was detrimental to enzymatic hydrolysis of cellulose.^{10,22} However, the direct effect of lignin surface structure after hydrothermal treatment on enzymatic hydrolysis has not been elucidated. It was thus studied if the presence of altered lignin formed during AH affected enzymatic cellulose-to-glucose conversion from the solid residue samples.

Fig. 3 (a) Lignin surface area (SA) and (b) specific surface area (SSA) in solid residues from autohydrolysis before (black circles) and after NH_3 (aq) extraction at moderate intensity (5% NH_3 , 140 °C, white rectangles) or high intensity (20% NH_3 , 160 °C, gray triangles) as a function of autohydrolysis severity. The error bars shown indicate average deviation from the mean values.

The effect of lignin surface area on enzymatic hydrolysis of cellulose

AH and NH_3 (aq) extractions of straw produced solid residues that contained altered levels of lignin surface area (SA). In order to elucidate the effect of lignin on enzymatic hydrolysis of cellulose, Klason lignin (KL) content or lignin SA of the solid residues was correlated with the degree of cellulose conversion. Increasing KL content showed a positive linear correlation after AH ($R^2 = 0.68$) and, in contrast, a weak negative correlation after successive NH_3 (aq) extraction (Fig. 4). The highest 24 h cellulose conversions (89% and 91%) resulted from AH at high severity ($\log R_0 = 4.1$ and $\log R_0 = 4.4$), despite the 13% and 30% higher lignin content in the solid residues relative to untreated WS (Table 1). This apparent contradiction of improved hydrolysis of cellulose in presence of higher amounts of lignin has not been completely understood before. However, degree of cellulose conversion from 24 h or 72 h hydrolysis of

Fig. 4 Cellulose-to-glucose conversion in 24 h (white circles) and 72 h (black circles) enzymatic hydrolysis of solid residues from autohydrolysis before (a) and after NH_3 (aq) extraction at moderate or high intensity (b) as a function of Klason lignin content of solid residues or as a function of lignin surface area (SA) (c and d). The error bars shown indicate average deviation from the mean values.

AH solid residues showed negative linear correlations ($R^2 = 0.92$, $R^2 = 0.97$) with lignin SA (Fig. 4). Similarly, NH_3 (aq) extractions also led to a negative correlation with SA (Fig. 4).

In contrast to prior indication that enzymatic digestibility is controlled by lignin content,²³ these results showed that lignin SA, rather than the lignin content, governs degree of cellulose conversion from AH solid residues. Prior to the current study, Kristensen and co-workers concluded that improved enzymatic digestibility was a result of re-localization of lignin and removal of hemicellulose rather than physical disruption of cell walls in hydrothermal treatment of WS.¹² More specifically, lignin probably undergoes complex changes involving phase-transition, reaction, and dissolution during hydrothermal pretreatment.²⁴ However, the nature of lignin surface properties after AH has not been elucidated with respect to cellulose hydrolysis before the current study. Extraction of AH solid residues with aqueous ammonia led mainly to lower enzymatic cellulose conversions than obtained without extraction (Table 1). This was despite delignification was the apparent result of the NH_3 (aq) extractions, showing enrichment of up to 74% cellulose in the solids residues (Table 1). Moreover, based on the SEM micrographs, solid residues after the NH_3 (aq) extractions contained defibrillated material that was absent in the AH solid residues (Fig. 2). NH_3 (aq) extraction improved cellulose conversion only after AH at low severity (Table 1). Thus, while the effect of lignin removal might be ascribed as formation of

additional cellulose surface area,²⁵ it appears in contrast that the most important factor of AH on cellulose hydrolysis is the reduction of lignin SA.

The effect of autohydrolysis and aqueous ammonia treatments on sugar yield

Sugar yield from lignocellulosic feedstock deserves a closer look with respect to the studied fractionation processes. Sugar yields were calculated from the two processes where prior to enzymatic hydrolysis, straw was subjected to AH only or AH with successive NH_3 (aq) extractions. If only the sugars released by enzymatic hydrolysis are considered, the maximum sugar yield (59%) was obtained from the single-stage AH at $\log R_0 = 3.81$ severity (Fig. 5a). When sugars in AH liquors¹¹ were additionally taken into account, up to 85% sugar yield was obtained from the process comprising AH only (Fig. 5b). The successive NH_3 (aq) extractions did not improve the sugar yield compared to the single-stage AH process, except after AH at the lowest severity.

Conclusions

High severity AH decreased the surface area of lignin in the solid residues almost by half compared to untreated straw, leading to nearly complete hydrolysis of cellulose. Extraction of AH solid residues with NH_3 (aq) increased the surface area of

Fig. 5 Sugar yield from wheat straw carbohydrates as a function of autohydrolysis severity with different process combinations prior to enzymatic hydrolysis of the solid fraction: autohydrolysis (gray circles), autohydrolysis followed by NH_3 (aq) extraction at moderate intensity (white rectangles) or high intensity (black triangles). Sugar yield based on sugar released only by enzymatic hydrolysis of solid residues (a) or the sum of sugar from enzymatic hydrolysis and sugar released in autohydrolysis¹¹ (b).

lignin in the solid residues. This unexpected finding was concluded to be the result of incomplete removal of lignin and especially the preferred removal of pseudo-lignin from the solid residues. While reduction of proportion of native lignin from lignocellulosic feedstock is often beneficial for enzymatic hydrolysis of cellulose, non-lignin-removing treatments that specifically decrease surface area of lignin are also expected to improve cellulose-to-glucose conversion. From the perspective of biofuel production, the surface area of lignin remaining in contact with cellulose appears a highly important parameter with respect to the enzymatic hydrolysis process.

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