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Enhanced polymer capture speed and extended translocation time in pressure-solvation traps

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The efficiency of nanopore-based biosequencing techniques requires fast anionic polymer capture by like-charged pores followed by a prolonged translocation process. We show that this condition can be achieved by setting a pressure-solvation trap. Polyvalent cation addition to the KCl solution triggers the like-charge polymer-pore attraction. The attraction speeds-up the pressure-driven polymer capture but also traps the molecule at the pore exit, reducing the polymer capture time and extending the polymer escape time by several orders of magnitude. By direct comparison with translocation experiments [D. P. Hoogerheide et al., ACS Nano 8, 7384 (2014)], we characterize as well the electrohydrodynamics of polymers transport in pressure-voltage traps. We derive scaling laws that can accurately reproduce the pressure dependence of the experimentally measured polymer translocation velocity and time. We also find that during polymer capture, the electrostatic barrier on the translocating molecule slows down the liquid flow. This prediction identifies the streaming current measurement as a potential way to probe electrostatic polymer-pore interactions.

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I. INTRODUCTION

The 21st century has brought the convergence of previously independent scientific disciplines with the aim of understanding complex structures. Biopolymer analysis by nanotechnological approaches is a clear example of this scientific turnover [1,2]. Along these lines, driven polymer translocation has recently undergone rapid progress [3–13]. Serial sequencing techniques that require the biochemical or mechanical modification of each molecule before sequencing.

The predictive design of polymer translocation devices necessitates primarily the characterization of the electrohydrodynamic and entropic effects governing this highly complex transport process. The entropic contributions from polymer conformations and steric polymer-pore interactions during translocation have been scrutinized by Brownian simulations [14–17] and the tension propagation theory [18–20]. The electrohydrodynamics of polymer translocation has been considered both by numerical simulations and continuum theories. Monte Carlo (MC) studies by Luan and Aksimentiev investigated the effect of the electroosmotic (EO) flow [21,22] and DNA mobility reversal by polyvalent counterions [23]. By Brownian simulations coupled with a Fokker-Planck (FP) approach, the authors of Ref. [24] analyzed the electrostatic barrier acting on polymers translocating through α-hemolysin pores. In Ref. [25], the effect of dipoles placed on the polymer surface was modeled with the aim of extending the translocation time of the molecule.

Theoretical formulations of purely voltage-driven polymer transport have been mostly based on mean-field (MF) Poisson-Boltzmann (PB) electrostatics and hydrodynamic Navier-Stokes equation. Along these lines, the pioneering drift transport theory developed by Ghosal allowed the consistent derivation of the DNA translocation velocity in terms of the electrophoretic (EP) and EO velocity components [26,27]. Ghosal’s midpore approximation was subsequently relaxed by Lu et al. via the numerical solution of the coupled PB and Stokes equations [28]. The effect of polymer-pore interactions on the unzipping of a DNA hairpin was studied in Ref. [29]. Wong and Muthukumar investigated the role played by the EO flow during diffusion-limited polymer capture by a positively charged pore [30]. Additional models considering the nonequilibrium dynamics of the translocation process on polymer capture [31,32] have been compared with experiments [33]. The details of the polymer hydrodynamics have been also investigated in Refs. [34–36] by continuum approaches. In Ref. [37], we characterized the correlation-corrected electrohydrodynamics of polymer translocation without the consideration of polymer-pore interactions. Then in Ref. [38], we incorporated into the electrohydrodynamic transport model of Ref. [27] the repulsive barrier originating from electrostatic polymer-pore interactions at the MF level. This improvement extended the drift formalism of Ref. [27] to include the barrier-limited capture regime prior to translocation. Finally, we have recently extended our purely voltage-driven translocation model of Ref. [38] beyond MF level and identified an electroosmotically facilitated polymer capture mechanism [39].

Polymers can alternatively be transported by an externally applied hydrostatic pressure gradient between the cis and trans sides of the membrane. The pressure gradient induces a streaming flow through the pore. The drag force exerted by this streaming current carries the polymer from the cis to trans side of the membrane. At the theoretical level, streaming flow-driven polymer transport has received less attention than its
electrohydrodynamic counterpart. Solving Edward’s polymer diffusion equation, Stein et al. studied entropic effects on polymer transport through nanoslits [40]. In Ref. [41], we predicted ionic correlation-induced streaming current inversion in pressure-driven polymer translocation events. At this point, we note that the precision of polymer translocation requires, among other factors, the extension of the translocation time on polymer capture [7]. Translocation experiments by Hoogerheide et al. showed that this goal can be achieved by setting a pressure-voltage trap, which consists of imposing a pressure gradient with the aim of counterbalancing the external voltage [12,13]. It was observed that the resulting suppression of the net drift force allows us to trap the translocating molecule without causing significant perturbation of the ionic current signal. Via the numerical solution of the electrohydrodynamic formalism of Ref. [28] coupled with an effective diffusion equation, the experimental data of translocation time was also interpreted in Ref. [13].

In this article, we characterize the additional effect of direct electrostatic polymer-membrane interactions in polymer translocation events driven by a pressure and a voltage. To this end, in Sec. II, we extend the voltage-driven transport model of Ref. [38] to include the streaming current induced by an applied pressure gradient. Section III deals with the electrohydrodynamic mechanism driving such a pressure-voltage trap. First, we confront our theory with the experiments of Ref. [13]. We show that our newly derived scaling laws (34) and (37) can quantitatively describe the experimentally measured evolution of the polymer translocation velocity and time with the pressure gradient. Then, in terms of the experimentally tunable system parameters, we fully characterize the polymer conductivity of anionic pores under pressure-voltage traps. Our theory also predicts that during polymer capture, like-charge polymer-pore interactions transmitted to the liquid by the drag force slow down the liquid flow. This suggests that the nature and magnitude of electrostatic polymer-pore interactions can be extracted from streaming current measurements.

In addition to a prolonged polymer translocation, the efficiency of nanopore-based sequencing methods requires fast polymer capture by the pore. Considering that most of the silicon-based solid-state pores carry negative surface charges of high density [8], the technical challenge consists in driving as fast as possible an anionic polymer into a like-charged pore by overcoming the electrostatic polymer-pore repulsion. In Sec. IV, we show that rapid polymer capture and extended translocation can be mutually achieved by setting a pressure-solvent trap driven by charge correlations. To this end, we generalize the formulation of polymer pore-interactions beyond the MF level. This extension is introduced within the test charge theory of Ref. [42] explained in Sec. IV A. We note that the test charge theory has been previously shown to accurately describe the experimentally observed similar charge attraction between polyelectrolytes [43,44] and polymer-membrane complexes [45,46].

Within this correlation-corrected pressure-driven transport formalism, we show that polyvalent cations added to the KCl solution amplify electrostatic correlations and turn polymer-pore interactions from repulsive to attractive. This like-charge attraction enhances the polymer capture speed but also traps the molecule at the pore exit, reducing the barrier-limited polymer capture time and extending the polymer escape time by several orders of magnitude. This result is the key prediction of our work. We note that a similar trapping mechanism resulting from the inversion of the fixed pore charge on pH variation has been experimentally observed in translocation events in α-hemolysin pores [47]. In terms of the experimentally controllable system parameters, we thoroughly identify the parameter regime maximizing the enhancement of the polymer capture speed and escape time by the electrostatic trap. It should be noted that this trapping mechanism differs from the facilitated polymer capture process of Ref. [39] where the polymer capture speed is enhanced by the EO flow rather than polymer-pore interactions. The approximations and possible improvements of our model are elaborated on under Conclusions.

II. TRANSLOCATION MODEL

Our translocation model is depicted in Fig. 1. The cylindrical nanopore of radius $d$, length $L_m$, and negative surface charge density $-\sigma_m$ is in contact with a reservoir containing the KCl electrolyte, a multivalent cation species of valency $q > 0$, and anionic polymers of low concentration whose interactions can be neglected. The reservoir concentration of the ionic species $i$ is $\rho_{bi}$, and the bulk electroneutrality reads $\rho_{b+} - \rho_{b-} + q\rho_{bq+} = 0$. The dielectric permittivities of the pore and the membrane are, respectively, $\epsilon_w = 80$ and $\epsilon_m = 2$. Considering that dsDNA has a large persistence length of about 50 nm, we neglect conformational polymer fluctuations. Thus, the translocating polymer is modelled as a rigid cylinder of length $L_p$ and typical radius $a = 1$ nm of dsDNA molecules. The discrete helicoidal charge distribution on the DNA backbone is approximated by a continuous surface charge density $-\sigma_p$, with the numerical value $\sigma_p = 0.4$ e/nm$^2$ previously obtained by fitting experimental current blockage data [37]. Polymer translocation from the cis to trans side occurs under the effect of the applied voltage $\Delta V$ and pressure $\Delta P$, and the
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potential barrier \( V_p(z_p) \) resulting from electrostatic polymer-membrane interactions.

The translocation dynamics is characterized by the polymer number density \( c(z_p,t) \) satisfying the Smoluchowski equation [31,48]

\[
\partial_t c(z_p,t) = - \partial_{z_p} J(z_p,t),
\]

\[
J(z_p,t) = - D \partial_{z_p} c(z_p,t) + v_p(z_p) r(z_p,t),
\]

where \( z_p \) is the position of the polymer with diffusion coefficient \( D = \ln(L_p/2a)/(3\pi \eta L_p \beta) \) \([49,50]\), with the inverse thermal energy \( \beta = 1/(k_B T) \), the Boltzmann constant \( k_B \), the liquid temperature \( T = 300 \) K, and the solvent viscosity \( \eta = 8.91 \times 10^{-3} \) Pa s. Furthermore, \( J(z_p,t) \) stands for the net polymer flux through the pore, with the polymer velocity

\[
v_p(z_p) = - \beta DU_p'(z_p),
\]

where \( U_p(z_p) \) is the polymer potential that will be derived below. At steady state with constant polymer density, \( \partial_t c(z_p,t) = 0 \), the integration of the uniform flux condition \( J(z_p,t) = J_0 \) together with the fixed density condition at the pore entrance \( c(z_p = 0) = c_cis \) and an absorbing boundary at the pore exit \( c(z_p = L_p + L_m) = 0 \) yields the polymer number density in the form

\[
c(z_p) = c_cis e^{-\beta U_p(z_p)} \int_{L_p+z_p}^{L_p+L_m} dz e^{\beta U_p(z)} \int_0^{L_m+L_p} dz e^{\beta U_p(z)}.
\]

Moreover, the translocation rate defined as the polymer current per density \( R_c \equiv J_0/c_cis \) follows as

\[
R_c = \frac{D}{\int_0^{L_m+L_p} dz e^{\beta U_p(z)}}.
\]

We finally note that in the dilute polymer regime where polymer interactions are negligible, the number density \( c(z_p) \) is equivalent to the polymer probability function.

The following part generalizes the electrohydrodynamic transport model of Ref. [38] to include the pressure gradient. In order to derive the polymer potential \( U_p(z_p) \), we introduce first the PB and Stokes equations for the electrostatic potential \( \phi(r) \) and convective fluid velocity \( u_c(r) \) in the pore,

\[
\frac{1}{r} \partial_r [r \partial_r \phi(r)] + 4\pi \epsilon_0 \chi [\rho_v(r) + \sigma(r)] = 0,
\]

\[
\frac{\eta}{r} \partial_r [r \partial_r u_c(r)] - \epsilon_0 \partial_r \phi(r) E + \frac{\Delta P}{L_m} = 0,
\]

with the radial distance \( r \) from the pore axis, the Bjerrum length \( l_B = e^2/(4\pi \epsilon_0 \epsilon_w) \), the electron charge \( e \), and the density of mobile charges \( \rho_v(r) = \sum_{i=1}^3 q_i \rho_{ib} e^{-\nu_i \phi(r)} \) and fixed charges \( \sigma(r) = -\sigma_0 \delta(r-d) - \sigma_p \delta(r-a) \). In Eqs. (6) and (7), the cylindrical symmetry of the model was preserved by neglecting electrohydrodynamic edge effects associated with the finite pore length. This approximation is justified by the fact that the pore and polymer lengths considered in our work are much larger than the Bjerrum length \( l_B \approx 7 \) Å corresponding to the spatial scale where finite electrohydrodynamic size effects on polymer capture would be relevant. In Sec. III.B, this point will be confirmed by comparison with experiments. Now, we combine the PB and Stokes Eqs. (6) and (7) to eliminate the density \( \rho_v(r) \), and integrate the result with the no-slip boundary condition at the pore wall \( u_c(d) = 0 \) and at the DNA surface \( u_c(a) = V_p(z_p) \). Finally, we account for Gauss’s law \( \phi(a) = 4\pi \epsilon_0 l_B \sigma_p \) and the force balance relation on the polymer \( F_{el} + F_{dr} + F_b = 0 \), with the electrostatic force \( F_{el} = 2\pi a L_p \mu e E \), the drag force \( F_{dr} = 2\pi a L_p \eta u_c(a) \), and the barrier-induced force \( F_b = -V_p(z_p) \). After some algebra, the liquid and polymer velocities follow as

\[
u_e(r) = \mu_e E[\phi(d) - \phi(r)] - \beta D_p(r) \frac{\partial V_p(z_p)}{\partial z_p},
\]

\[
u_p(z_p) = \nu_{dr} - \beta D_p(a) \frac{\partial V_p(z_p)}{\partial z_p},
\]

with the effective diffusion coefficient in the pore

\[
D_p(r) = \frac{\ln(d/r)}{2\pi \eta L_p \beta}.
\]

EP mobility coefficient \( \mu_e = e_\omega k_B T/(e \eta) \), and the drift velocity component

\[
\nu_{dr} = \frac{\mu_e \Delta V}{L_m} \left[ \phi(d) - \phi(a) \right] + \frac{\gamma a^2 \Delta P}{4\eta L_m},
\]

where

\[
\gamma = \frac{d^2}{a^2} - 1 - 2 \ln \left( \frac{d}{a} \right),
\]

Combining Eqs. (3) and (9), and integrating the result, the effective polymer potential that determines the density (4) finally becomes

\[
U_p(z_p) = \frac{D_p(a)}{D} V_p(z_p) - \frac{\nu_{dr}}{\beta D_p(z_p)}.
\]

In Eq. (13), the interaction potential corresponds to the electrostatic coupling energy between the fixed pore and polymer charges,

\[
V_p(z_p) = \Delta \Omega_p l_p(z_p),
\]

where \( \Delta \Omega_p(l_p) \) stands for the electrostatic grand potential of the polymer portion located in the pore. The position-dependent length of this portion reads

\[
l_p(z_p) = z_p \theta(L_- - z_p) + L_- \theta(z_p - L_-) \theta(L_+ - z_p) + (L_p + L_m - z_p) \theta(z_p - L_+),
\]

with the auxiliary lengths

\[
L_- = \min(L_m, L_p); \quad L_+ = \max(L_m, L_p).
\]

The explicit form of the polymer grand potential \( \Delta \Omega_p(l_p) \) in Eq. (14) will be specified in Secs. III and IV according to the approximation level.

III. PRESSURE-VOLTAGE TRAPS

We characterize here the pressure-voltage-driven translocation of polymers in the monovalent KCl solution of reservoir concentration \( \rho_b \). Electrostatic correlations being negligible in monovalent electrolytes, charge interactions will be formulated within MF electrostatics.

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A. Computation of the drift velocity and electrostatic barrier

According to Eq. (11), the computation of the drift velocity $v_d$ in Eq. (13) requires the knowledge of the pore potential $\phi(r)$. In the cylindrical pore geometry, the corresponding PB Eq. (6) does not possess a closed-form solution. Within an improved Donnan approximation that allows us to preserve the nonlinearity of Eq. (6), the pore potential was derived in Ref. [38] in the form

$$\phi(r) = -\ln(t + \sqrt{t^2 + 1}) + \frac{8\pi \ell_B \sigma_m d + \sigma_p a}{\kappa_d^2} \cdot$$

$$+ \frac{4\pi \ell_B}{\kappa_d} \int I_1(k_d r) \frac{T_1 I_0(k_d r) + T_2 K_0(k_d r)}{I_1(k_d a) K_1(k_d d) - K_1(k_d a) I_1(k_d d)}.$$

In Eq. (17), we introduced the ratio of the membrane and pore charge densities $t = (d \sigma_m + a \sigma_p)/[\rho_0 (d^2 - a^2)]$, the auxiliary coefficients $T_1 = \sigma_m K_1(k_d a) + \sigma_p K_1(k_d d)$ and $T_2 = \sigma_m I_1(k_d a) + \sigma_p I_1(k_d d)$ with the modified Bessel functions $I_n(x)$ and $K_n(x)$ [51], and the effective pore screening and bare Debye-Hückel parameters

$$\kappa_d = \kappa_0 \left(1 + \frac{r^2}{\ell^2}\right)^{1/4}; \quad \kappa_b = \sqrt{8\pi \ell_B \rho_0}.$$

Inserting the potential (17) into Eq. (11), the drift velocity becomes

$$v_d = \frac{4\pi \ell_B \mu_e}{\kappa_d L_m} \Theta \Delta V + \frac{\gamma a^2 \Delta P}{4 \eta L_m},$$

with the auxiliary coefficient

$$\Theta = \frac{T_1 I_0(k_d a) K_1(k_d d) - T_2 K_0(k_d a) I_1(k_d d)}{I_1(k_d a) K_1(k_d d) - K_1(k_d a) I_1(k_d d)}.$$

The MF level interaction energy between the polymer portion in the pore and the fixed pore charges reads

$$\beta \Delta \Omega_p(l_p) = \int d\mathbf{r}_p \phi_p(\mathbf{r}).$$

The polymer charge density is

$$\sigma_p(\mathbf{r}) = -\sigma_p \delta(r - a) \theta(\mathbf{r} - \mathbf{z}).$$

The electrostatic potential $\phi_m(r)$ induced exclusively by the pore charges follows from Eq. (17) by setting $\sigma_p = 0$,

$$\phi_m(r) = -\ln(t_m + \sqrt{t_m^2 + 1}) + \frac{d}{\mu_m \kappa_m^2} \frac{K_1(k_m a) I_0(k_m a) + I_1(k_m a) K_0(k_m a)}{I_1(k_m a) K_1(k_m d) - K_1(k_m a) I_1(k_m d)}.$$

with the charge ratio $t_m = d \sigma_m/[\rho_0 (d^2 - a^2)]$, the screening parameter $\kappa_m = \kappa_0 (1 + t_m^2)^{1/4}$, and the Gouy-Chapman-Lenhart parameter $\mu_m = 1/(2\pi \ell_B \sigma_m)$. Substituting the charge density (22) into Eq. (21), the interaction potential (14) finally becomes

$$V_p(z_p) = -2\pi a \sigma_p k_B T \phi_m(\mathbf{z}_p).$$

In an anionic pore where $\phi_m(a) < 0$, the potential (24) rises with the penetration length $l_p$. Thus, this potential acts as an electrostatic barrier that limits the polymer capture. Finally, introducing the characteristic inverse lengths associated with the drift (19) and the barrier (24),

$$\lambda_d = \frac{v_d \ell_B}{D}; \quad \lambda_b = -2\pi a \sigma_p \phi_m(a) \frac{D_p(a)}{D},$$

the polymer velocity (9) and potential (13) follow as

$$v_p(z_p) = v_d - D \lambda_b \left[\theta(L_m - z_p) - \theta(z_p - L_m)\right],$$

$$\beta U_p(z_p) = \lambda_b l_p(z_p) - \lambda_d z_p.$$

B. Comparison with trapping experiments

Using the polymer density function (4) and Eqs. (26) and (27), we calculate first the average polymer velocity

$$\langle v_p \rangle = \frac{\int_{0}^{L_p + L_m} dz_p v_p(z_p) w_p(z_p)}{\int_{0}^{L_p + L_m} dz_p w_p(z_p)}.$$

Carrying out the integrals in Eq. (28), one obtains

$$\langle v_p \rangle = v_d - D \lambda_b \frac{J_1 - J_3}{J_1 + J_2 + J_3},$$

where the coefficients $J_i, i = 1,2,3$ depending on the parameters $\lambda_d,\lambda_b$ and $L_\pm$ are reported in Appendix. In Fig. 2(a), we display the pressure dependence of the velocity (29) together with the experimental velocity data of Ref. [13]. The experimental parameters taken from Ref. [13] are the voltage $\Delta V = -100$ mV, the salt density $\rho_0 = 1.6$ M, the monomer number $N = 615$ bps corresponding to the polymer length $L_p = 180$ nm, and the pore radius $d = 5$ nm. The pore length and charge density were adjusted to the values $L_m = 200$ nm [52] and $\sigma_m = 0.13 e/nm^2$ that provided the best agreement with the magnitude of the velocity data. The charge density value is comparable with the experimental value $\sim 30$ mC/m$^2 \approx 0.18 e/nm^2$ measured at the solution pH $\approx 8$ [53] where the translocation experiments of Ref. [13] were carried out.

FIG. 2. (a) Average polymer velocity $\langle v_p \rangle$ and (b) translocation time $t_p = (L_m + L_p)/\langle v_p \rangle$ versus pressure. Solid curves are from Eq. (29) and squares mark the linear result (30). The experimental velocity data in (a) are from Fig. S3 of the supplemental information of Ref. [13]. The data of average escape time in (b) are from Fig. 4(b) of Ref. [13]. The model parameters are given in the main text.
In the barrier-driven regime $\lambda_b \gg \lambda_d$, Eq. (29) simplifies to $\langle v_p \rangle \approx D(\lambda_d - \lambda_b)$. Passing to the linear PB approximation, and expanding the inverse lengths of Eq. (25) in terms of $\sigma_p$ and $\sigma_m$, the velocity follows as

$$\langle v_p \rangle \approx \frac{f_p \sigma_p - f_m \sigma_m}{g} \frac{e \Delta V}{L_m} + \frac{g^2 \sigma_p \sigma_m \ln (d/a)}{4 \eta L_m} - \frac{e \sigma_p \sigma_m \ln (d/a)}{g \eta \epsilon \kappa_b L_p},$$

(30)

where we introduced the geometric coefficients

$$f_p = K_1(\kappa_b d) I_0(\kappa_b d) - I_1(\kappa_b d) K_0(\kappa_b d),$$

(31)

$$f_m = K_1(\kappa_b d) I_0(\kappa_b d) + I_1(\kappa_b d) K_0(\kappa_b d),$$

(32)

$$g = I_1(\kappa_b d) K_1(\kappa_b d) - I_1(\kappa_b d) K_1(\kappa_b d).$$

(33)

The approximation (30) derived in the barrier-dominated regime will be shown to work as well in the drift-driven regime $\lambda_b \ll \lambda_d$, where $\langle v_p \rangle \approx D\lambda_d \approx D(\lambda_d - \lambda_b)$.

The first component of Eq. (30) accounts for the EP drift (positive term) and the EO drag (negative term). The second and third components originate respectively from the streaming current, and the electrostatic barrier induced by like-charge polymer-membrane repulsion that hinders the polymer capture. Equation (30) reported in Fig. 2(a) indicates that as the ion density rises the polymer velocity ($\rho_b \uparrow \langle v_p \rangle \uparrow$) and switches its sign from negative to positive. Thus, added salt favors polymer capture. In order to gain analytical insight into this effect, we expand Eq. (30) in the corresponding strong salt regime $\kappa a \gg 1$ and $k d \gg 1$ to obtain

$$\langle v_p \rangle \approx \frac{(\sigma_p - \sigma_m) e \Delta V}{\eta L_m \kappa_b} + \frac{\gamma a^2 \Delta P}{4 \eta L_m}.$$

(34)

According to Eq. (38), the velocity increase by added salt originates from the screening of the voltage-induced drift opposing the polymer capture. Due to the same screening effect, in Fig. 3(b) where polymer transport is driven by voltage ($\Delta V > 0$), added salt of high density ($\rho_b \gtrsim 0.1$ M) turns the velocity from positive to negative ($\rho_b \uparrow \langle v_p \rangle \downarrow$) and blocks polymer transport. Setting Eq. (38) to zero, the ion concentration for polymer trapping in strong salt follows as

$$\rho_{b>\ast} \approx \frac{2}{\pi \ell_B} \left[ \frac{(\sigma_p - \sigma_m) e \Delta V}{\gamma a^2 \Delta P} \right]^2.$$

(39)

A successful translocation requires the polymer to travel the distance $L_m + L_p$. The translocation time can thus be estimated in terms of the velocity (29) as

$$\tau_p \approx \frac{L_m + L_p}{\langle v_p \rangle}. \quad (36)$$

Figure 2(b) shows that with the same parameters as in Fig. 2(a), this theoretical estimation can accurately reproduce the experimental escape times of Ref. [13]. The linear PB approximation for $\tau_p$ obtained from Eq. (34)

$$\tau_p \approx \frac{4 \eta L_m (L_p + L_m)}{\gamma a^2 (\Delta P - \Delta P^*)} \quad (37)$$

indicates that the quick rise of the experimental escape time with decreasing pressure occurs according to an inverse power law (see the square symbols).

C. Effect of salt, polymer length, and pore size

We scrutinize here the effect of the experimentally tuneable parameters on polymer trapping. Figures 3(a) and 3(b) illustrate the salt dependence of the polymer velocity and also show the accuracy of the approximation (30) (square symbols). In Fig. 3(a) where translocation is driven by the streaming current ($\Delta P > 0$) and limited by voltage ($\Delta V < 0$), the increment of the ion density rises the polymer velocity ($\rho_b \uparrow \langle v_p \rangle \uparrow$) and switches its sign from negative to positive. Thus, added salt favors polymer capture. In order to gain analytical insight into this effect, we expand Eq. (30) in the corresponding strong salt regime $\kappa a \gg 1$ and $k d \gg 1$ to obtain

$$\langle v_p \rangle \approx \frac{(\sigma_p - \sigma_m) e \Delta V}{\eta L_m \kappa_b} + \frac{\gamma a^2 \Delta P}{4 \eta L_m}.$$  

According to Eq. (38), the velocity increase by added salt originates from the screening of the voltage-induced drift opposing the polymer capture. Due to the same screening effect, in Fig. 3(b) where polymer transport is driven by voltage ($\Delta V > 0$), added salt of high density ($\rho_b \gtrsim 0.1$ M) turns the velocity from positive to negative ($\rho_b \uparrow \langle v_p \rangle \downarrow$) and blocks polymer transport. Setting Eq. (38) to zero, the ion concentration for polymer trapping in strong salt follows as

$$\rho_{b>\ast} \approx \frac{2}{\pi \ell_B} \left[ \frac{(\sigma_p - \sigma_m) e \Delta V}{\gamma a^2 \Delta P} \right]^2.$$  

(39)

In agreement with Figs. 3(a) and 3(b), Eq. (39) predicts the decrease of the characteristic salt density with increasing pressure gradient, i.e., $|\Delta P| \uparrow \rho_{b>\ast} \downarrow$.

In the dilute salt regime of Fig. 3(b), one notes the presence of a second critical salt density where the velocity cancels. To explain the origin of this reversal point, we expand Eq. (30) for $\kappa a \ll 1$ and $k d \ll 1$ to get

$$\langle v_p \rangle \approx \frac{(a_p \sigma_p - a_m \sigma_m) e \Delta V}{\eta L_m} + \frac{\gamma a^2 \Delta P}{4 \eta L_m} - \frac{d a \ln (d/a) k_B \tau_p \sigma_p \sigma_m}{d^2 - a^2 \eta L_p \rho_b}.$$  

(40)

with the auxiliary coefficients

$$a_p = -a + \frac{ad^2 \ln (d/a)}{d^2 - a^2}; \quad a_m = \frac{d}{2} - \frac{a^2 \ln (d/a)}{d^2 - a^2}. \quad (41)$$
Equation (40) indicates that in Fig. 3(b), enhanced polymer conductivity by added salt ($\rho_b \uparrow \langle v_p \rangle \uparrow$) stems from the screening of repulsive polymer-membrane interactions. Thus, polymer trapping at dilute salt originates from the competition between the drift force and the electrostatic barrier. The corresponding salt concentration follows from Eq. (40) as

$$\rho_{bc} \approx \frac{4 \ln(d/a)L_m}{(d^2 - a^2)L_p} \frac{k_BT \sigma_p \sigma_m}{\gamma a^2 a^2 \Delta P + 4(a_p \sigma_p - a_m \sigma_m) e \Delta V}.$$

(42)

In accordance with Fig. 3(b), Eq. (42) predicts the rise of the lower critical salt concentration by enhanced negative pressure, i.e., $|\Delta P| \uparrow \rho_{bc} \uparrow$.

The phase diagrams of Figs. 3(c) and 3(d) illustrate the salt dependence of the critical pressure (35). One sees that regardless of the voltage sign, the critical pressure is reduced by dilute salt, i.e., $\rho_b \uparrow \Delta P^* \downarrow$. The low ion density expansion of Eq. (35)

$$\Delta P^* \approx -\frac{4(a_p \sigma_p - a_m \sigma_m)}{\gamma a^2} e \Delta V + \frac{4 \ln(d/a) \sigma_p \sigma_m L_m}{\beta \gamma a^2 (d^2 - a^2)L_p \rho_b}$$

(43)

indicates that this behavior results from the screening of the electrostatic barrier. In voltage-driven transport ($\Delta V > 0$), this trend is reversed in the strong salt regime where the critical pressure rises, $\rho_b \uparrow \Delta P^* \uparrow$. The high density expansion of Eq. (35)

$$\Delta P^* \approx -\frac{4(a_p \sigma_p - a_m \sigma_m) e \Delta V}{\gamma a^2 k_B}$$

(44)

shows that the rise of $\Delta P^*$ is due to the shielding of the voltage-induced drift force on DNA.

We consider now the effect of the finite polymer length. According to Eq. (43), in the dilute salt regime, the capture of shorter polymers requires higher pressures, i.e., $L_p \downarrow \Delta P^* \uparrow$. This finite-size effect is also displayed in Figs. 3(c) and 3(d). The obstruction of polymer capture by finite molecular length is due to the repulsive barrier term of Eq. (30); the streaming current and voltage act on the whole polymer of length $L_p$ while the barrier affects solely the polymer portion in the pore. Hence, the net drag force on the polymer decreases with the length of the molecule. As a result, the polymer velocity (30)

drops with decreasing polymer length ($L_p \downarrow \langle v_p \rangle \downarrow$) as

$$\langle v_p \rangle \approx u_d \left(1 - \frac{L_p^*}{L_p}\right),$$

(45)

with the critical molecular length for polymer trapping

$$L_p^* = \frac{4 e^2 \sigma_p \sigma_m \ln(d/a)L_m}{\gamma a^2 \Delta P + 4(a_p \sigma_p - a_m \sigma_m) e \Delta V}.$$

(46)

Figure 4(a) shows that the competition between the barrier and the streaming current results in the decay of the length (46) with pressure, i.e., $\Delta P \uparrow L_p^* \downarrow$. As depicted in the same figure, the dilute salt expansion of Eq. (46),

$$L_p^* \approx \frac{4 \ln(d/a)L_m}{(d^2 - a^2) \rho_b} \frac{k_BT \sigma_p \sigma_m}{\gamma a^2 \Delta P + 4(a_p \sigma_p - a_m \sigma_m) e \Delta V},$$

(47)

predicts that the same competition leads to the decay of the critical length with added salt, i.e., $\rho_b \uparrow L_p^* \downarrow$.

During polymer capture ($z_p < L_p$), the electrostatic barrier also affects the liquid velocity. For the sake of simplicity, we consider a purely pressure-driven polymer transport and set $\Delta V = 0$. The linear PB limit of Eq. (8),

$$u_e(r) = \frac{\Delta P}{4 \eta L_p} \left[d^2 - r^2 - 2a^2 \ln \left(\frac{d}{r}\right)\right] - \frac{\sigma_p \sigma_m}{g \eta \beta \rho_b L_p} \ln \left(\frac{d}{r}\right),$$

(48)

shows that the barrier slows down the streaming flow around the DNA molecule. This effect is illustrated in Fig. 4(b). The decrease of the polymer length enhances the barrier and reduces the fluid velocity below the Poiseuille profile (black curve), $L_p \downarrow u_e(r) \downarrow$. Below the critical length $L_p = L_p^* \approx 160$ nm, the velocity of the polymer and the surrounding liquid becomes negative. This prediction suggests that the magnitude of the electrostatic polymer-membrane interactions can be extracted from the streaming current blockade in pressure-driven translocation events.

We finally investigate the effect of pore confinement. Figure 4(c) shows that as a result the barrier attenuation, at positive pressures $\Delta P \geq 0$, the polymer velocity uniformly rises with the pore radius, $d \uparrow \langle v_p \rangle \uparrow$. The reduction of the translocation time with increasing pore radius has been observed in voltage-driven translocation experiments [10]. Then, at negative pressures $\Delta P < 0$, the velocity initially rises, reaches a peak, and...
decays at large pore radii \( (d \uparrow (v_p) \downarrow) \) where the streaming current opposing the polymer capture overcomes the EP drift. The cancellation of the polymer velocity at two different pore radii is an observation of practical significance for the design of polymer trapping devices.

**IV. PRESSURE-SOLVATION TRAPS**

In nanopore-based biosensing approaches, the improvement of the sequencing precision necessitates the mutual enhancement of the capture speed and translocation time [3,7,8]. Here, we show that in purely pressure-driven translocation, this goal can be achieved by adding polyanion cations to the KCl solution. At vanishing voltage \( \Delta V = 0 \) where the drift velocity (11) simplifies to

\[
V_d = \frac{\gamma a^2 \Delta P}{4\eta L_m},
\]

(49)
electrostatic interactions come into play only through the interaction potential \( V_p(\zeta_p) \) in Eq. (13). In the presence of polyanvlar charges, the derivation of this potential requires the computation of the polymer grand potential \( \Delta \Omega_p(l_p) \) beyond MF electrostatics. Section IV A reviews the inclusion of the corresponding charge-correlations within the one-loop (11) test charge theory developed in Refs. [42,44].

### A. Correlation-corrected grand potential

In the 11 test charge theory, the correlation-corrected polymer grand potential is calculated by approximating the enhancement of the capture speed and translocation time [3,7,8]. The polymer grand potential is obtained by expanding the polymer charge density \( \sigma_p(r) \) given by Eq. (22). This expansion yields [44]

\[
\Delta \Omega_p(l_p) = \Delta \Omega_{\text{MF}}(l_p) + \Delta \Omega_p(l_p),
\]

(50)
with the MF component accounting for the direct electrostatic coupling between the polymer and pore charges

\[
\beta \Delta \Omega_{\text{MF}}(l_p) = \int dr \sigma_p(r) \phi_m(r),
\]

(51)
and the polymer self-energy bringing 11-level electrostatic correlations

\[
\beta \Delta \Omega_p(l_p) = \frac{1}{2} \int d^3 r \sigma_p(r)[v(r,r') - v_p(r-r')]\sigma_p(r'),
\]

(52)
The MF-level grand potential component (51) includes the polymer charge density (22) and the membrane-induced potential \( \phi_m(r) \) solving the PB equation

\[
\frac{1}{4\pi \varepsilon_B} \partial_t \phi_m(r) + \sum_{i=1}^3 \rho_{bij} q_i e^{-q_i \phi_p(r)} = \sigma_m \delta(r-d).
\]

(53)
Equation (53) cannot be solved in a closed form. The improved Donnan solution of this equation was derived in Ref. [42] in the form

\[
\phi_m(r) = \phi_d + \frac{4\pi \varepsilon_B \sigma_m}{\kappa_d} \left[ \frac{I_0(\kappa_d r)}{I_1(\kappa_d r)} \right],
\]

(54)
where the Donnan potential \( \phi_d \) and screening parameter \( \kappa_d \) are obtained from the relations

\[
\sum_{i=1}^3 \rho_{bij} q_i e^{-q_i \phi_d} = 2\sigma_m, \quad \kappa_d^2 = \frac{4\pi \varepsilon_B}{2\sum_{i=1}^3 \rho_{bij} q_i^2 e^{-q_i \phi_d}}.
\]

(55)
Substituting the potential (54) into Eq. (51), one obtains

\[
\beta \Delta \Omega_{\text{MF}}(l_p) = l_p \psi_{\text{MF}},
\]

(56)
with the dielectric permittivity function \( \epsilon(r) = \epsilon_w \theta(d-r) + \epsilon_m \theta(r-d) \) and the local screening parameter

\[
k^2(r) = 4\pi \varepsilon_B \sum_{i=1}^3 \rho_{bij} q_i^2 e^{-q_i \phi_d(r)} \delta(d-r).
\]

(59)
Equation (52) also contains the bulk Green’s function \( \psi_b(r) = \ell_B e^{-|r|/\ell_B} \), where the bulk screening parameter is

\[
k_b^2 = 4\pi \varepsilon_B \sum_{i=1}^3 \rho_{bij} q_i^2.
\]

(60)

In Ref. [42], Eq. (58) was solved within a Wentzel-Kramers-Brillouin (WKB) approach and the self-energy (52) was obtained in the form

\[
\beta \Delta \Omega_p(l_p) = l_p \psi_p(l_p),
\]

(61)
with the self-energy per polymer length

\[
\psi_{p}(l_p) = \ell_B \tau^2 \int_{-\infty}^{\infty} dk \frac{2 \sin^2(kl_p/2)}{\pi \ell_p k^2} \left\{ \ln \left[ \frac{p_b}{p(0)} \right] + \frac{Q(k)}{P(k)} \right\}.
\]

(62)
The auxiliary functions in Eq. (62) are defined as

\[
Q(k) = 2 \rho^3(-d) d B_0(k) K_0(|k|d) K_1(0) [B_0(0)]
\]

\[
- \frac{2}{\kappa^2} \rho^2 k^2 B_0(k) K_1(|k|d) K_0(0),
\]

\[
- \frac{[P^3(-d) d P^2(0) B_0(k) - \kappa^2 d \kappa^2 B_0(0)]}{ \times K_0(|k|d) K_0(0)},
\]

(63)
\[
P(k) = 2 \rho^3(-d) d B_0(k) K_0(|k|d) I_1(0) K_1(0) [B_0(0)]
\]

\[
+ \frac{2}{\kappa^2} \rho^2 k^2 B_0(k) K_1(|k|d) I_0(0),
\]

\[
+ \frac{[P^3(-d) d P^2(0) B_0(k) - \kappa^2 d \kappa^2 B_0(0)]}{ \times K_0(|k|d) I_0(0)},
\]

(64)
with the dielectric contrast parameter \( \gamma = \varepsilon_\text{p} / \varepsilon_\text{w} \), the screening parameter \( p_b = \sqrt{k_b^2 + \kappa_b^2} \), and the functions \( p(r) = \sqrt{k_b^2 + \kappa_b^2(r)} \) and \( B_b(r) = \int_0^r \kappa_b^2 \, dr' \, p'(r') \).

In anionic pores characterized by a cation excess, one has \( p(0) > p_b \). Consequently, the logarithmic term of the self-energy (62) is negative. Thus, this attractive solvation component favors polymer capture [54]. Then the second term of Eq. (62) originating from polymer-image-charge interactions is repulsive and limits polymer penetration. Taking now into account Eq. (15), the polymer-pore interaction potential (14) can be finally expressed in terms of the polymer grand potential (50) as

\[
V_p(z_p) = \Delta \Omega_p(l_p) = z_p \theta(L_m - z_p) + \Delta \Omega_p(l_p) = L_m - z_p \theta(L_m - z_p) + \Delta \Omega_p(l_p) = L_p + L_m - z_p \theta(L_p - z_p) + \Delta \Omega_p(l_p) = L_p + L_m - z_p \theta(L_p - z_p) + \Delta \Omega_p(l_p) = L_p + L_m - z_p \theta(L_p - z_p). \tag{65}
\]

**B. Computing translocation time**

In the presence of strong polymer-pore interactions, the drift approximation (36) for the polymer translocation time ceases to be accurate. Thus, we derive here the general form of the translocation time. By plugging Eq. (3) into Eqs. (1) and (2), the polymer diffusion equation takes the form of a Fokker-Planck equation

\[
\frac{\partial c(z_p,t)}{\partial t} = D_\text{z_p} \frac{\partial^2}{\partial z_p^2} c(z_p,t) + \beta D_\text{z_p} [c(z_p,t)U_p'(z_p)]. \tag{66}
\]

In the translocation process characterized by Eq. (66), the mean first passage time \( \tau_p(z_2; z_1) \) from the initial point \( z_1 \) to the final point \( z_2 \) solves the equation \([48]\)

\[
D_\text{z_p} \frac{\partial}{\partial z_p} \tau_p(z_2; z_1) - \beta D_\text{z_p} U_p(z_1) \tau_p(z_2; z_1) = -1. \tag{67}
\]

Solving Eq. (67) with reflecting and absorbing boundary conditions, respectively, at the points \( z_1 = 0 \) and \( z_2 = L_m + L_p \), the translocation time follows as

\[
\tau_p(t) = \tau_c(t) + \tau_d(t) + \tau_e(t), \tag{68}
\]

where the capture, pore diffusion, and escape times are, respectively,

\[
\tau_c(t) = I_t(0, L_m), \tag{69}
\]

\[
\tau_d(t) = I_t(L_m, L_m), \tag{70}
\]

\[
\tau_e = I_t(L_m, L_p + L_m), \tag{71}
\]

with the auxiliary integral

\[
I_t(z_i, z_f) = \frac{1}{D_\text{z_p}} \int_{z_i}^{z_f} \int_0^{z_i} \int_0^{z_f} d z'' e^{-\beta U_p(z'')}. \tag{72}
\]

**C. Faster polymer capture and longer translocation on Spm\(^4\)+ addition**

We consider the effect of spermine (Spm\(^4\)+) molecules on polymer capture and translocation. Figures 5(a) and 5(b) illustrate the polymer translocation rates and times versus the Spm\(^4\)+ concentration of the electrolyte KCl + SpmCl\(_4\). Figures 5(c) and 5(d) display in turn the polymer-pore interaction and effective potential profiles. In the density regime \( \rho_{b+} \ll 10^{-4} \), the addition of Spm\(^4\)+ molecules to the KCl solution enhances the translocation rate and reduces the translocation time, i.e., \( \rho_{b+} \uparrow R_c \uparrow \tau_p \downarrow \). The increase of the translocation speed is induced by the onset of the like-charge polymer-pore attraction; Spm\(^4\)+ molecules screen the repulsive MF-level electrostatic barrier (57) and amplify the attractive component of the self-energy (62). Figures 5(c) and 5(d) show that this switches the interaction potential \( V_p(z_p) \) from repulsive to attractive and turns the polymer potential \( U_p(z_p) \) to downhill (compare the black and blue curves).

Enhancing further the Spm\(^4\)+ density from \( \rho_{b+} = 10^{-4} \text{ M} \) (blue dots) to \( 10^{-3} \text{ M} \) (purple dots), the translocation time rises together with the translocation rate, i.e., \( \rho_{b+} \uparrow R_c \uparrow \tau_p \uparrow \). This intriguing disconnection between the translocation rate and time originates from the solvation-induced trapping of the polymer. Added Spm\(^4\)+ molecules amplify the like-charge DNA-pore attraction. This enhances the depth of the interaction potential \( V_p(z_p) \) and the effective potential \( U_p(z_p) \) develops a minimum at \( z_p = L_m \) (see the purple curves in Figs. 5(c) and 5(d)). Thus, the like-charge DNA-membrane attraction that speeds up the polymer capture also traps the molecule at the pore exit. The consequence of this trapping mechanism on the characteristic times (69)–(71) is illustrated in Fig. 6(a). The increment of the Spm\(^4\)+ density from \( \rho_{b+} = 10^{-5} \text{ M} \) to \( 10^{-3} \text{ M} \) reduces the polymer capture time and amplifies the escape time \( \tau_p \) by several orders of magnitude. This result is the key prediction of our work.

Rising the bulk Spm\(^4\)+ density beyond the value \( \rho_{b+} \approx 10^{-3} \text{ M} \), charge screening weakens the pore potential \( \phi_p(r) \) and the Spm\(^4\)+ excess in the pore. Figures 5(c) and 5(d) show that this attenuates the like-charge DNA-pore attraction and removes the minimum of the effective potential (see the red curves). In Fig. 5(b), one sees that the removal of the trap at \( \rho_{b+} \gtrsim 10^{-3} \text{ M} \) results in the decrease of the translocation time, i.e., \( \rho_{b+} \uparrow \tau_p \downarrow \). One also notes that due to the screening of the like-charge attraction, the weak rise of the monovalent salt density reduces the trapping time \( \rho_{b+} \uparrow \tau_p \downarrow \) by orders of
D. Characterization of the barrier, drift, and trapping regimes

In order to gain a quantitative insight into the features discussed in Sec. IV C, we evaluate analytically the characteristic times (69)–(71) against the Spm4\textsuperscript{+} density. In (a), the squares and dots mark respectively the asymptotic laws (81) and (83) on their validity regime. The monovalent salt density is $\rho_{bs+} = 13$ mM and the pressure gradient $\Delta P = 2$ atm. The other parameters are the same as in Fig. 2.

The effect of Spm4\textsuperscript{+} molecules on the translocation time can be quantitatively characterized in terms of the inverse lengths $\lambda_b$ and $\lambda_d$. Their ratio corresponding to the adimensional interaction potential is displayed in Fig. 6(b). In the barrier-driven regime $\lambda_b > \lambda_d$ corresponding to the spermine density range $\rho_{bs+} \lesssim 10^{-5}$ M, the expansion of Eqs. (78)–(80) for $\lambda_d / \lambda_b < 1$ yields the characteristic time hierarchy $\tau_c \gg \tau_d \gg \tau_p$ and

$$\tau_p \approx \tau_c \approx \frac{e^{(\lambda_b - \lambda_d)L_+}}{D(\lambda_b - \lambda_d)^2}. \quad (81)$$

Thus, the capture time is the dominant characteristic time of the barrier-driven regime. The asymptotic law (81) reported in Fig. 6(a) by square symbols corresponds to the Kramer’s reaction rate for polymer capture by overcoming the barrier $U_b = k_B T (\lambda_b - \lambda_d)L_-$.

Figures 6(a) and 6(b) show that as one rises the Spm4\textsuperscript{+} density beyond $\rho_{bs+} \approx 10^{-5}$ M, the removal of the electrostatic barrier $U_b$ reduces sharply the capture time (81) and drives the system into the drift-dominated regime $\lambda_b > \lambda_d > -\lambda_d$. Indeed, in the strict limit $|\lambda_b| / \lambda_d \ll 1$, the expansion of Eqs. (78)–(80) yields the limiting law

$$\tau_p \approx \tau_d = \frac{L_m + L_p}{v_dr}, \quad (82)$$

indicating purely drift-driven transport at velocity $v_dr$. Equation (82) is displayed in Fig. 6(a) by the purple curve.

In Fig. 6(b), one sees that the increase of the Spm4\textsuperscript{+} density further beyond the value $\rho_{bs+} \approx 10^{-3.5}$ M drives the system into the trapping regime $\lambda_b < -\lambda_d$. Expanding Eqs. (78)–(80) for $\lambda_b / \lambda_d < -1$, one gets $\tau_c \gg \tau_d \gg \tau_p$ and

$$\tau_p \approx \tau_c \approx \frac{-\lambda_b}{D(\lambda_b + \lambda_d)^2} e^{-(\lambda_b + \lambda_d)L_+}. \quad (83)$$

Hence, in the trapping regime, the escape time dominates the translocation. The asymptotic law (83) displayed in Fig. 6(a)
by circles corresponds to the reaction rate for the unbinding of the polymer from the pore exit where the molecule is trapped in a potential well of depth \( U_b = k_B T |\lambda_b + \lambda_d| L_p \).

In this regime, the abrupt rise of the escape time \((83)\) on Spm\(4^+\) addition stems precisely from the lowering of the trap depth \( U_b \) by the intensification of the like-charge polymer-pore attraction.

At this point, the question arises whether the solvation-induced trapping can be induced by counterions of lower valency. Figure 7(a) displays the polymer capture and escape times in three different electrolyte mixtures KCl + ICl\(_m\). Each solution has a different bulk K\(^+\) density indicated in the caption. The figure shows that as long as the monovalent salt concentration of the liquid is lowered together with the valency of the multivalent cation species I\(^\text{m+}\), trivalent Spd\(^{3+}\), and divalent Mg\(^{2+}\) counterions can reduce the capture time and extend the escape time as efficiently as quadrivalent Spm\(^{4+}\) molecules. In Fig. 7(b), this point is illustrated in terms of the peak translocation time versus the monovalent salt density. One notes that the lower the valency of the polyelectrolyte counterion species, the lower the K\(^+\) density range where the maximum translocation time rises sharply.

In Fig. 6, the correlation between \( \tau_p \) and \( \lambda_b / \lambda_d \) indicates that the polyelectrolyte cation density \( \rho_{b\text{m*}} \) maximizing the trapping time can be evaluated by identifying the minimum of the grand potential (77).

To progress further, we consider the Gouy-Chapman (GC) regime of dilute salt \( \kappa_b \mu \ll 1 \) with the GC length \( \mu = 1/(2\pi \ell_g \sigma_m) \). Expanding the equalities in Eq. (55), at leading order, the Debye potential and screening parameter follow as \( \phi_d \approx -\ln [2\sigma_m/(m\rho_{b\text{m*}} + d)]/m \) and \( \kappa_d^2 \approx 8\pi \ell_g m \sigma_m/|d| \). Substituting these equalities into Eq. (84) and carrying out another expansion for \( \kappa_b \mu \ll 1 \), the grand potential density finally becomes

\[
\psi_{\text{tot}} \approx -\frac{\tau}{m} \ln \left( \frac{2\sigma_m}{m\rho_{b\text{m*}} + d} \right) - \frac{\ell_g}{2} \ln \left\{ \frac{2m\sigma_m}{d(2\rho_{b\text{m*}} + (m^2 + m)\rho_{b\text{m*}})} \right\}.
\]

The density \( \rho_{b\text{m*}} \) maximizing the translocation time \( \tau_p \) follows from the equation \( \partial \psi_{\text{tot}} / \partial \rho_{b\text{m*}} = 0 \) as

\[
\rho_{b\text{m*}}^* = \frac{4\rho_{b\text{m}}}{(m^2 + m)(m\ell_g \tau - 2)}.
\]

In the derivation of the density (86), the system was assumed to be in the trapping regime. This requires both the polymer self-energy and the grand potential (85) to be negative. Thus, the polymer charge density should satisfy the inequality \( \tau > 2/(m\ell_g) \). Figure 7(c) illustrates the numerically evaluated characteristic density \( \rho_{b\text{m*}}^* \) (solid curves) together with the analytical estimation (86) (dots). Equation (86) indicates that \( \rho_{b\text{m}} \) rises linearly with the K\(^+\) concentration \( \rho_{b\text{m*}} \) and drops rapidly with the polyelectrolyte counterion valency according to an inverse cubic polynomial law \((m \uparrow \rho_{b\text{m}} \downarrow)\).

Finally, we characterize finite-size effects on polymer trapping. By equating the characteristic inverse lengths in Eq. (76), the critical polymer length separating the drift and interaction-dominated regimes follows as

\[
L_p^* = \frac{2\ln(d/a) L_m}{\pi \beta \gamma a^2 \Delta P} |\psi_{\text{tot}}|.
\]

Figure 7(d) displays Eq. (87) against the Spm\(^{4+}\) density. The transition from the drift-driven \((L_p > L_p^*)\) to the barrier/trapping regime \((L_p < L_p^*)\) on polymer length reduction stems from the decrease of the pressure-induced drag force on the polymer. The corresponding balance between polymer-pore interactions and the drift force was scrutinized in Sec. III C for monovalent solutions.

In the dilute Spm\(^{4+}\) regime of Fig. 7(d) characterized by repulsive polymer-pore interactions \((\psi_{\text{tot}} > 0)\), added Spm\(^{4+}\) molecules suppress the electrostatic barrier and lower the critical length, i.e., \( \rho_{b\text{m*}} \uparrow \left| \psi_{\text{tot}} \right| \downarrow L_p^* \downarrow \). In the subsequent Spm\(^{4+}\) density range where the like-charge polymer-pore
attraction is activated ($\psi_{tot} < 0$), Spm$^{4+}$ addition enhances the trapping potential depth and rises the critical polymer length, $\rho_{b4+} ↑ |\psi_{tot}| ↑ L^*_P ↑$. Beyond the density value $\rho_{b4+} \approx 1$ mM, added Spm$^{4+}$ molecules screen the attractive polymer-pore interactions. This reduces the depth of the potential trap and drops the critical length. To conclude, polymer trapping by like-charge attraction occurs if the polymer length satisfies the condition $L_P < L^*_P$. The upper polymer length (87) can be, however, tuned by controlling the magnitude of the potential $\psi_{tot}$ via the alteration of the ion density.

V. CONCLUSIONS

The optimization of polymer translocation techniques requires the accurate characterization of the electrohydrodynamic forces governing driven polymer transport. In this article, we characterized the collective effect of the EP drift, the drag force induced by the streaming flow, and electrostatic polymer-pore interactions on polymer translocation through solid-state pores. Our main results are summarized below.

In the first part, we investigated the polymer conductivity of pressure-voltage traps in monovalent salt solutions. By direct comparison with experimental data, we showed that our theory can accurately reproduce and explain the pressure dependence of the polymer translocation velocity and time. Then, we characterized the effect of salt density variation. In translocation events driven by streaming flow ($\Delta P > 0$) and limited by voltage ($\Delta V < 0$), added salt screens the negative EP mobility and favors polymer capture. In the opposite case of voltage-driven ($\Delta V > 0$) and pressure-limited translocation ($\Delta P < 0$), the polymer mobility exhibits a nonmonotonal salt dependence; dilute salt screens electrostatic polymer-pore interactions and favors polymer capture but strong salt reduces the EP mobility and blocks polymer transport. This nonuniform behavior results in the trapping of the polymer at two distinct salt density values given by Eqs. (39) and (42).

We also found that during polymer capture, the repulsive polymer-pore coupling can reduce or even invert the direction of the streaming current. Due to the amplification of the barrier effect, the reduction of the liquid velocity becomes stronger with decreasing polymer length. This suggests that electrostatic polymer-pore interactions can be probed by streaming current measurements carried-out at different polymer lengths.

The precision of polymer sequencing by translocation is known to depend on the fast capture of the polymer by a like-charged pore followed by a slow translocation. In the second part of our work, we identified an electrostatic polymer trapping mechanism that allows us to achieve this condition by the simple addition of polyvalent cations to the KCl solution. Enhanced electrostatic correlations on Spm$^{4+}$ addition turn the polymer-pore interactions from repulsive to attractive. This like-charge polymer-pore attraction results in a faster polymer capture from the cis side but traps the molecule at the pore exit on the trans side of the membrane. As a result, the increment of the Spm$^{4+}$ density from $\rho_{b4+} = 10^{-3}$ M to $10^{-3}$ M reduces the capture time and extends the escape time ($\rho_{b4+} ↑ \tau_e \downarrow \tau_c ↑$) by five orders of magnitude.

Provided that the monovalent salt density is lowered together with the valency of the polyvalent counterions, trivalent Spd$^{3+}$ and divalent Mg$^{2+}$ cations can trap the polymer as efficiently as quadrivalent Spm$^{4+}$ molecules. Equation (86) indicates that the polyvalent ion density $\rho_{bav}^*$ minimizing the capture time and maximizing the trapping time rises with the monovalent salt concentration $\rho_{b1+}$ and drops with the ionic valency $m ↑ \rho_{bav}^* ↓$. Finally, we showed that solvation-induced polymer trapping can be achieved only if the molecular length is below the critical length $L^*_P$ given by Eq. (87). It should be noted that the maximum length $L^*_P$ can be tuned by the alteration of the ion density.

Our formalism neglects some features of these highly complex systems, such as conformational polymer fluctuations [55], entropic barriers limiting polymer capture [15], the discrete charge distribution on the membrane surface, and the helicoidal charge partition on the polymer [56]. Our translocation model does not include either the interaction of the membrane with the polymer portion outside the pore, as well as hydrodynamic and electrostatic edge effects occurring at the pore ends [57]. Although the consequence of these approximations cannot be estimated quantitatively without the explicit inclusion of the corresponding effects, the agreement with experimental data indicates that in the experimental configuration considered herein, these complications play a secondary role. For example, as discussed in Sec. II, the accuracy of the stiff polymer approximation is due to the short length of the DNA sequences involved in the translocation experiments of Ref. [13]. It should be also noted that in the low-pressure regime of Fig. 2 where the net drift force on DNA becomes rather weak, entropic effects expected to become relevant may be responsible for the slight deviation of our theoretical curves from the experimental trend. In order to understand the electrohydrodynamics of translocation for long polymer sequences, at the first step, we plan to include to our model the interaction of the membrane matrix with the polymer portion outside the pore. At the next step, the inclusion of conformational polymer fluctuations will allow us to take into account the tension propagation mechanism introduced by Sakaue [18–20]. We finally note that our results and conclusions can be corroborated by current polymer transport experiments. In particular, the polyvalent cation-induced trapping can be easily verified by standard pressure-driven translocation experiments carried out with anionic nanopores. Our numerous predictions can also guide the optimized conception of new generation biosensing tools.

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APPENDIX: COEFFICIENTS OF THE AVERAGE POLYMER VELOCITY FORMULA (29)

We list here the coefficients of the average velocity formula (29) of the main text,

\[
J_1 = \frac{1}{(\lambda_d - \lambda_b)^2} \left[ (\lambda_d - \lambda_b) L_+ + e^{-(\lambda_d - \lambda_b) L_-} - 1 \right] + \frac{1}{\lambda_d - \lambda_b} \left[ 1 - e^{-(\lambda_d - \lambda_b) L_-} \right] \left[ \frac{1}{\lambda_d} \left[ 1 - e^{-\lambda_b (L_+ - L_-)} \right] + \frac{1}{\lambda_d + \lambda_b} e^{-(\lambda_d - \lambda_b) L_-} \left[ 1 - e^{-\lambda_b (L_+ - L_-)} \right] \right],
\]

(A1)

\[
J_2 = \frac{1}{\lambda_d} \left[ (\lambda_d - \lambda_b) (L_+ - L_-) + e^{-(\lambda_d - \lambda_b) (L_+ - L_-)} - 1 \right] + \frac{1 - e^{-(\lambda_d + \lambda_b) L_-}}{\lambda_d (\lambda_d + \lambda_b)} \left[ 1 - e^{-\lambda_b (L_+ - L_-)} \right],
\]

(A2)

\[
J_3 = \frac{1}{(\lambda_d + \lambda_b)^2} \left[ (\lambda_d + \lambda_b) L_- + e^{-(\lambda_d + \lambda_b) L_-} - 1 \right].
\]

(A3)

[52] The parameter $L_m$ corresponds to the position of the effective pore boundary where the polymer is removed from the system.

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on the trans side. Complications associated with the electrohydrodynamic edge effects at the pore ends, the deviation of the pore geometry from a perfect cylinder, and the variation of the electric field outside the pore are adsorbed into the effective parameter \( L_m \).


[54] The logarithmic term of Eq. (62) takes into account the enhanced screening ability of the pore medium with respect to the reservoir. This locally enhanced screening mechanism originating from the mobile charge excess drives as well the like-charge attraction between polymers [43,44] and polymer-membrane complexes [45,46].

